



PILOT PLANT IN SVEDALA

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Background – R&D in Sweden

For four years, from 2014 to 2017, the Swedish Agency for Marine and Water Management was assigned by the government to promote advanced treatment of wastewater by supporting projects in order to develop treatment methods for municipal treatment plants.

[Treatment techniques for pharmaceuticals and micropollutants in wastewater - Publications - Swedish Agency for Marine and Water Management \(havochvatten.se\)](#)

Treatment techniques for pharmaceuticals and micropollutants in wastewater

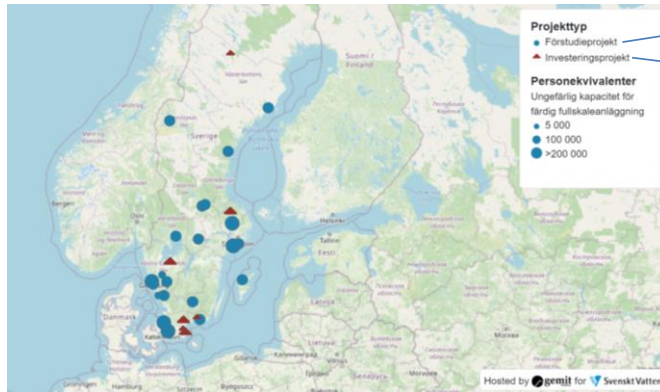
Description of eight projects that have received funding from the Marine and Aquatic Environment Grant for 2014-2017



Swedish Agency for Marine and Water Management report 2018:7

Background

Swedish EPA are supporting pre-studies and investments in full-scale plants



Feasibility studies

Full-scale investments

www.svensktvatten.se

Involved in Swedish pilot plant

- Lund University, Department of Chemical Engineering
- Sweden Water Research AB
- Kristianstad University
- Svedala Municipality (hosting the plant)



sweden  water research



SVEDALA KOMMUN



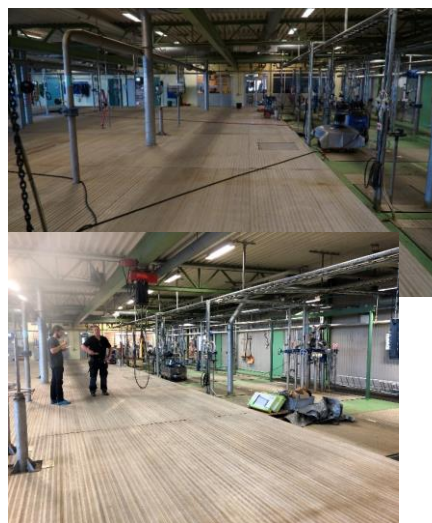
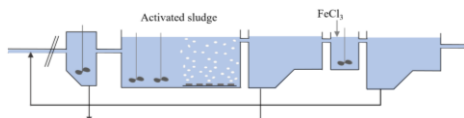
Wastewater treatment plant in Svedala

Loading: 12 000 PE (mainly domestic WW)

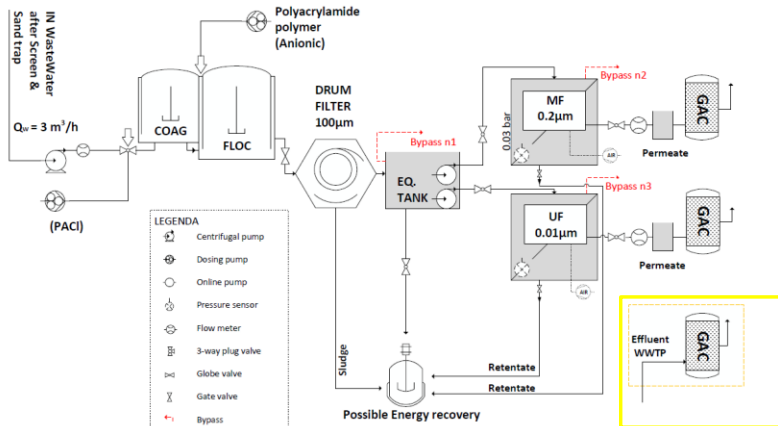
Biological and chemical wastewater treatment:

- No primary treatment
- Activated sludge (pre-denitrification)
- Post precipitation (FeCl_3) and tertiary settling

No anaerobic digestion of sludge



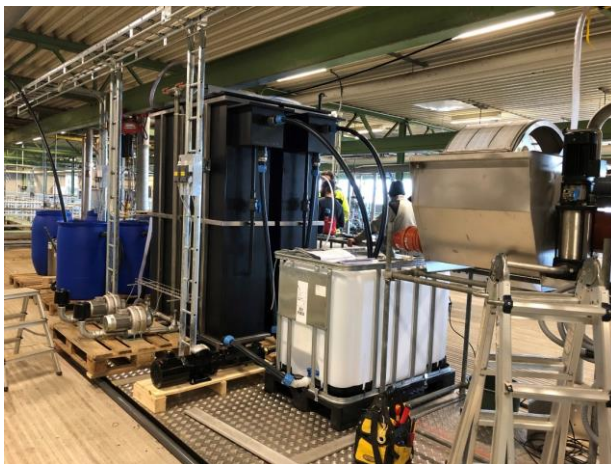
Pilot plant in Svedala



Two test lines:

- 1) Influent wastewater to direct membrane filtration (DMF) + GAC
- 2) Biologically treated wastewater to sand filter + GAC

Direct membrane filtration and GAC in Svedala



Membrane unit



GAC columns



Direct membrane filtration and GAC in Svedala

By introducing microsieving and membranes early in the process line an improved treatment process and enhanced potential for reuse of energy and water could be expected

- Wastewater treatment → high energy consumption
- Adding removal of organic micropollutants → even higher energy consumption

Instead: separate organic matter and use it for generation of energy (biogas production) and add GAC at the end

Municipal wastewater treatment by microsieving, microfiltration and forward osmosis
Concepts and potentials

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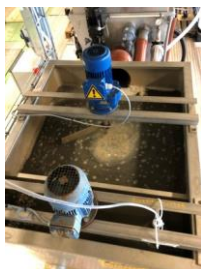


Technical data

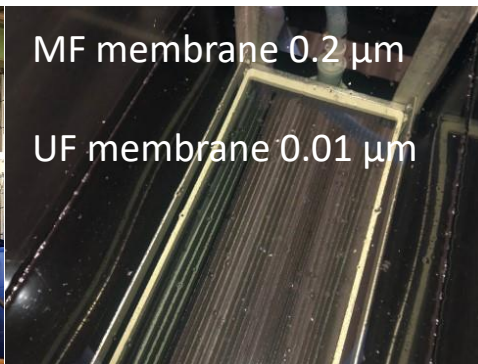
	Direct membrane filtration + GAC	Effluent GAC-filtration
Chemically Enhanced Primary Treatment (CEPT with filtration)	Coagulation tank (m ³)	0.2
	Flocculation tank (m ³)	0.8
	Coagulant dosing	In pipe (5-15 mg Al ³⁺ /L)
	Coagulant ^a	Polyaluminium chloride
	Polymer dosing	Overflow to flocc. tank (1-4 mg/L)
	Polymer ^b	Anionic
	Drum filter ^c area (m ²)	0.33
	Pore filter opening (μm)	100
	Filtration rate ^d (m/h)	8-9
	Equalization tank volume (m ³)	0.6
Direct Membrane Filtration	Membrane tank dimensions (m)	H: 2.35, W: 0.5, D: 1.5
	Membrane surface area (m ²)	40
	Cut-off (MWCO) UF ^e (Da)	10 000
	Pore size MF ^f (μm)	0.2
	Design flux ^d (L/m ² ·h ⁻¹)	25
	GAC column height (m)	0.54
GAC Filtration	GAC column volume (L)	19
	GAC cross section area (m ²)	0.04
	Mass of carbon ^g per column (kg)	5.98
	EBCT ^h (min)	10

Chemically Enhanced Primary Filtration

CEPT based on microsieving previously developed (in cooperation) at Lund University



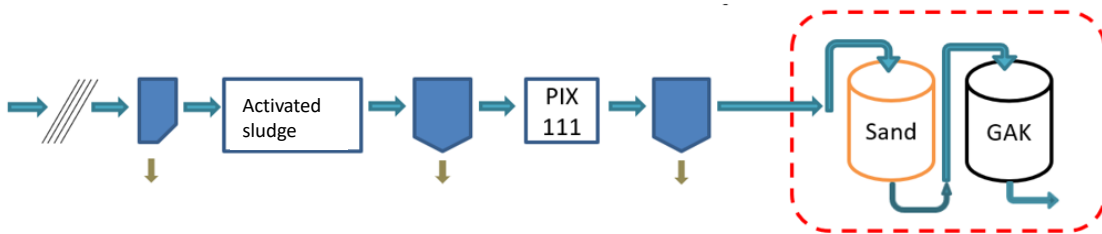
Membrane filtration



GAC columns



Effluent WW → Sand filter + GAC

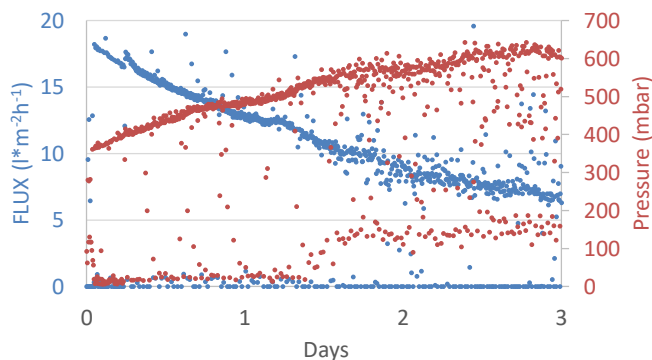
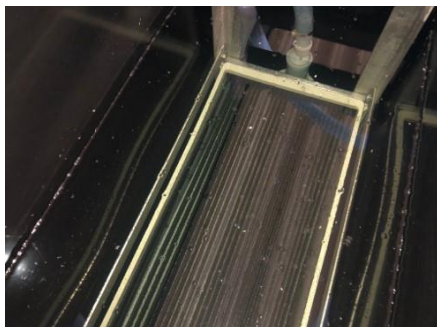


MoLab, Högskolan Kristianstad
Öje Byggnad och Erland Bygghuset

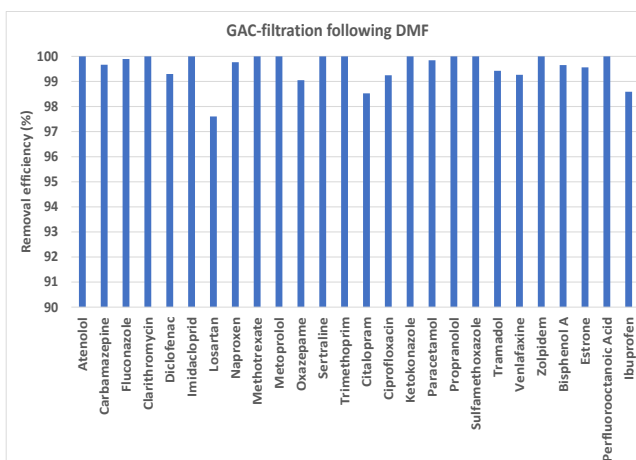
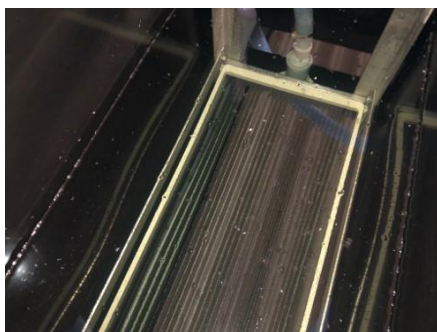
A bar chart comparing the percentage reduction of four parameters (COD, TOC, Ptot, and Ntot) using two different filtration methods: Microsieve (blue bars) and Microsieve + Ultrafiltration membrane (orange bars). The y-axis represents the percentage reduction from 0 to 100. The x-axis lists the parameters. For COD, TOC, and Ptot, the reduction is high, with the Ultrafiltration membrane showing slightly higher values than the Microsieve alone. For Ntot, the reduction is significantly lower for both methods, with the Ultrafiltration membrane showing a higher reduction than the Microsieve alone.

Parameter	Microsieve (%)	Microsieve + Ultrafiltration membrane (%)
COD	~88	~92
TOC	~80	~88
Ptot	~98	~100
Ntot	~28	~35

Fouling of membranes → no long-term operation of GAC

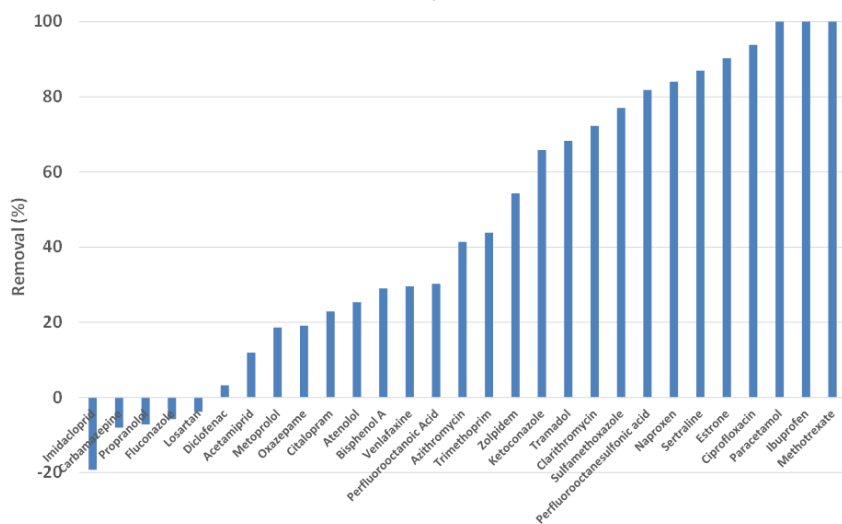


Short-term operation of GAC after UF



Short-term GAC after UF → 98-100%
removal of organic micropollutants
No removal in membrane filtration part

Removal efficiency Svedala WWTP



Results – effluent GAC

	3000 BV	8000 BV	18000 BV	22600 BV
Metoprolol	96%	97%	81%	50%
Losartan	84%	72%	42%	27%
Atenolol	97%	97%	75%	48%
Diclofenac	87%	74%	47%	27%
Tramadol	96%	94%	60%	37%
Carbamazepine	95%	91%	63%	40%
Venlafaxine	96%	92%	58%	38%
Oxazepam	93%	86%	60%	34%
Citalopram	99%	98%	88%	71%
Naproxen	86%	80%	48%	25%
Erythromycin	100%	69%	29%	-18%
Trimethoprim	97%	97%	91%	51%
Bisphenol A	79%	87%	71%	35%
Sulfamethoxazole	84%	60%	17%	-44%
Propranolol	98%	98%	94%	74%
Fluconazole	79%	65%	38%	19%
Sertraline	100%	100%	100%	100%
Ketokonazole	100%	100%	100%	85%
Imidacloprid	91%	93%	65%	38%
Clarithromycin	100%	80%	72%	-13%

Supplementary studies

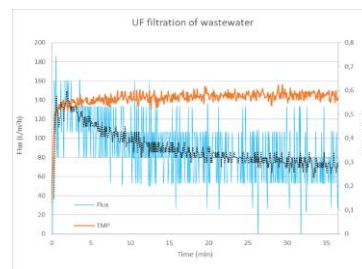
Differentiation between adsorption and degradation

Competition for adsorption onto activated carbon

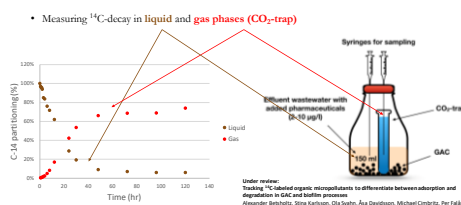
In-depth of a GAC filter

Evaluation of energy re-use

Water re-use potential



Degradation or adsorption in GAC?



QUESTIONS?

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